

1 **REVISION 1**

2 **The solubility of CePO<sub>4</sub> monazite and YPO<sub>4</sub> xenotime in KCl-H<sub>2</sub>O fluids at 800°C and 1.0 GPa:**  
3 **Implications for REE transport in high-grade crustal fluids**

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12  
13 **Abstract**

14 Monazite (CePO<sub>4</sub>) and xenotime (YPO<sub>4</sub>) are important hosts for REE, and thus can be used to monitor  
15 REE mass transfer in a variety of settings. In this investigation, the solubilities of synthetic monazite and  
16 xenotime were measured in KCl-H<sub>2</sub>O fluids at 800°C and 1.0 GPa, using the piston-cylinder apparatus.  
17 The experimental results indicate an increase in monazite and xenotime solubility in aqueous fluids with  
18 moderate KCl mole fractions (X<sub>KCl</sub>) in agreement with previous investigations of the solubility of these  
19 phases in NaCl-H<sub>2</sub>O. Under all conditions, monazite and xenotime dissolve congruently. The solubility of  
20 synthetic monazite increases from 8 ppm in pure H<sub>2</sub>O to 335 ppm at X<sub>KCl</sub> = 0.506. The solubility of  
21 synthetic xenotime rises from 46 ppm in pure H<sub>2</sub>O to 126 ppm at X<sub>KCl</sub> = 0.348, above which it is constant  
22 or declines slightly. Monazite and xenotime solubilities are considerably lower in KCl-H<sub>2</sub>O than in NaCl-  
23 H<sub>2</sub>O at the same salt concentration. Best fit equations for the solubilities of the two phases are:

24  $c_{mz} = -464 X_{KCl}^2 + 891 X_{KCl} + 8$

25 and

$$c_{xt} = -563 X_{KCl}^2 + 432 X_{KCl} + 46$$

where mz and xt stand for monazite and xenotime, and  $X_{KCl} = n_{KCl} / (n_{KCl} + n_{H_2O})$  where n is moles. The change in solubilities with KCl implies that Ce dissolves as an anhydrous chloride complex ( $CeCl_3$ ), whereas Y forms a mixed Cl-OH solute ( $YCl(OH)_2$ ). The data also imply that  $H_2O$ -NaCl fluids and  $H_2O$ -KCl fluids close to neutral pH can transport substantial amounts of REE and Y, thus obviating the need to invoke low pH solutions in high-grade environments where they are highly unlikely to occur.

**Keywords:** Monazite, Xenotime, Solubility, Experimental petrology, REE mobility, Metamorphic fluids, Brines

## Introduction

Aqueous fluids are responsible for substantial mass transfer in high pressure (P) and temperature (T) environments. Understanding the scale and magnitude of fluid-mediated compositional change is central to many studies of magmatic and metamorphic systems and ore deposits such as REE-enriched iron oxide-apatite deposits (cf. Harlov et al., 2016) or REE-enriched carbonatites (e.g., Yang et al., 2003). For example, lithologies transported to deep-crustal conditions along Barrovian P-T paths show evidence for significant compositional modification by metamorphic fluids (e.g., Ague, 1994a,b). Similarly, in subduction zones, slab devolatilization generates a fluid phase that is capable of major metasomatic activity (e.g., Manning, 2004). High-pressure (P) and temperature (T) environments (e.g., Barrovian and granulite metamorphism, and subduction zones) often record evidence of mobilization of elements that show very low solubility in  $H_2O$ , such as Al, Ti, and rare-earth elements (REE). Explanations may involve extremes in pH or complexing with halogens, alkalis, or both or polymerization with alkalis, Al and Si (e.g., Manning, 2004; Newton and Manning, 2010; Tropper et al., 2011; Tropper et al., 2013). A number of observations point to the participation of brines in high-grade metamorphic processes. These include not only findings of alkali and alkaline-earth halides as daughter crystals in fluid inclusions, but also

51 appreciable concentrations of Cl measured in minerals from high-grade rocks such as amphiboles, biotite,  
52 scapolite and apatite, and direct observations on high-temperature halides present in the intergranular  
53 space in high-grade rocks (e.g. Aranovich et al., 2014). Saline fluids may also be important in subduction-  
54 zone metasomatism (Barnes et al., 2017; Keppler, 2017).

55 Accessory minerals are minor in abundance, but can contain elements as major components (for example  
56 Ce in monazite and Y in xenotime), which with respect to the whole rock would be considered trace  
57 elements. If these minerals are part of the solid assemblage, their solubility will govern the abundance of  
58 key trace elements in co-existing fluids, including Ti, Nb, Ta, Zr, Hf, and REE. Therefore knowledge of  
59 rare earth element (Y+REE) redistribution during high-grade metamorphism is of fundamental importance  
60 in determining the origin of typical light (L)REE-enrichment of calc-alkaline magmas, commonly  
61 ascribed to the metasomatic effects of a subducting slab on the overlying mantle wedge (e.g., Ionov and  
62 Hofmann, 1995; Rubatto and Hermann, 2003; Gao et al., 2007). It is therefore essential to understand the  
63 behavior of (Y+REE) carriers such as monazite and xenotime during that metasomatic processes that  
64 attend high-grade metamorphism and subduction.

65 Monazite and xenotime are important accessory phases in metamorphic and igneous rocks (e.g., Spear and  
66 Pyle, 2002). Occurring over a range of metamorphic lithologies, settings, and P-T conditions, these  
67 phosphates have great utility as prograde index minerals that can be used for geochronology (e.g.,  
68 Harrison et al., 2002) and geothermometry (e.g., Gratz and Heinrich, 1997; Janots et al., 2008). They  
69 represent important reservoirs for light (LREE) and heavy (Y+HREE) rare earth elements. The exchange  
70 of (Y+REE) between orthophosphates and silicates, such as garnet, provides information concerning the  
71 P-T history of metamorphic terranes (e.g., Spear and Pyle, 2002). Y+REE orthophosphates also play an  
72 important role in controlling the distribution of (Y+REE), U, and Th during granitoid crystallization (e.g.,  
73 Montel, 1993). Their high durability and resistance to metamictization make the (Y+REE) phosphates  
74 potential hosts for nuclear waste disposal (e.g., Ewing, 2001). The mobility of REE in crustal and mantle  
75 fluids are especially important because of their role in REE ore-deposit formation (e.g., Williams-Jones et

76 al., 2012; Harlov et al., 2016) as well as their contribution in tracing magmatic (e.g., Markl and Piazzolo,  
77 1998; Agangi et al., 2010) and metamorphic (e.g., Yardley, 1985; Brennan, 1993) petrogenetic processes.  
78 Potassium metasomatism has been recognized by field workers in high-grade metamorphic terranes for  
79 over a century (e.g. Billings, 1938). Alkali exchange in natural feldspars (K-feldspathization) gives rise to  
80 “replacement antiperthite”, a common texture in high-grade gneisses (Todd and Evans, 1994; Hansen et  
81 al., 1995). Potassium species are also important constituents of high-grade metamorphic fluids (e.g.,  
82 Aranovich and Newton, 1997; Newton et al., 1998; Harlov and Förster, 2002a; Harlov, 2012) and  
83 potassium metasomatism has been recognized in high-grade metamorphic terranes (e.g., Hansen et al.,  
84 1995; Newton et al., 1998; Harlov et al., 1998; Harlov and Förster, 2002a; Harlov, 2012). KCl brines or  
85 K-rich also act as metasomatic fluids in xenoliths from the lower crust and upper mantle (Harlov and  
86 Davies, 2004), Kimberlites (Kamenetsky et al., 2004), as well as brine-rich inclusions in diamonds  
87 (Tomlinson et al., 2004). Sylvite (KCl) has been identified as a daughter mineral in some of the  
88 concentrated brine inclusions which have been described with increasing frequency in many petrogenetic  
89 settings, including granites (Dunbar et al., 1996), gabbros (Pasteris et al., 1995), high-grade gneisses  
90 (Touret, 1985), carbonatites (Sampson et al., 1995), eclogites (Philippot and Selverstone, 1991), and the  
91 super-high-pressure coesite-bearing metasediments (Philippot et al., 1995). KCl is thought to have been a  
92 major solute of the complex saline fluids which produced regional metasomatism and metal ore  
93 segregation in Cloncurry, Queensland (DeJong and Williams, 1995) and the Melones Fault Zone of  
94 California (Albino, 1995). The role of KCl-NaCl-H<sub>2</sub>O-rich fluids has also been investigated in a number  
95 of experimental studies on the relationship between activity and concentration (Aranovich and Newton,  
96 1997), the stability of phlogopite (Aranovich and Newton, 1998), fluid-induced dehydration of tonalites  
97 (Harlov, 2004; Harlov et al., 2006) and biotite-amphibole gneiss (Safonov et al., 2012), monazite/apatite  
98 dissolution-precipitation (Harlov and Förster, 2003; Harlov et al., 2005), quartz solubility (Shmulovich  
99 et al., 2005), and brine-assisted anatexis (Aranovich et al., 2014).

100 Despite their importance as minerals whose occurrence as prograde index minerals can be coupled with

101 geochronology (e.g. Janots et al., 2009) and their economic importance (Williams-Jones et al., 2012;  
102 Harlov et al., 2016), little is known about the solubility systematics of two of the most important  
103 orthophosphate REE-bearing minerals, monazite ( $\text{CePO}_4$ -) and xenotime ( $\text{YPO}_4$ -) in aqueous fluids of  
104 various compositions at high P ( $> 0.5$  GPa) and T ( $> 300$  °C). It is therefore essential to understand their  
105 solubility behavior with respect to P-T- $X_i$  conditions and complexation during metasomatic processes that  
106 attend high-grade crustal metamorphism and crustal/mantle/rock-fluid interactions occurring during  
107 subduction.

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### Experimental methods

110 Solubility experiments involving solutions with varying concentrations of KCl were conducted on  
111 synthetic crystals of monazite ( $\text{CePO}_4$ ) and xenotime ( $\text{YPO}_4$ ), and natural monazite from a beach sand in  
112 Cleveland Co., North Carolina (UCLA mineral collection #MS 1762), which contains 59.96 wt% LREE  
113 (29.41 wt%  $\text{Ce}_2\text{O}_3$ , 13.44 wt%  $\text{La}_2\text{O}_3$ , 11.15 wt%  $\text{Nd}_2\text{O}_3$ , 3.08 wt%  $\text{Pr}_2\text{O}_3$ , 1.87 wt%  $\text{Sm}_2\text{O}_3$  and 1.01 wt%  
114  $\text{Gd}_2\text{O}_3$ ) and 0.76 wt% HREE (with 0.55 wt%  $\text{Y}_2\text{O}_3$ , 0.08 wt%  $\text{Dy}_2\text{O}_3$ , 0.07 wt%  $\text{Tb}_2\text{O}_3$ , 0.02 wt%  $\text{Ho}_2\text{O}_3$ ,  
115 0.02 wt%  $\text{Er}_2\text{O}_3$  and 0.02 wt%  $\text{Yb}_2\text{O}_3$ ) (Tropper et al., 2011).

116 Synthetic crystals of monazite ( $\text{CePO}_4$ ) or xenotime ( $\text{YPO}_4$ ) were synthesized by mixing stoichiometric  
117 amounts of  $\text{REE}(\text{NO}_3)_6 \cdot 6\text{H}_2\text{O}$  and  $(\text{NH}_4)_2\text{HPO}_4$  in solution. The resulting precipitate was allowed to settle  
118 and the excess fluid poured off. The precipitate was then dried and ground. Twenty grams of Pb-free flux  
119 ( $\text{Na}_2\text{CO}_3:\text{MoO}_3 = 1:3$ ) mixed with 0.8 g precipitate was packed in a Pt crucible with a loose cover and  
120 heated to 1280 °C. The molten flux was allowed to equilibrate at 1280 °C for 15 h, and then cooled to 870  
121 °C at 3 °C per hour (Cherniak et al., 2004; Tropper et al., 2011). The resulting transparent, light brownish  
122 yellow, euhedral to semi-euhedral monazite and xenotime crystals range from 0.1 mm to 2 mm in  
123 diameter. The smaller crystals are inclusion-free, but some of the larger crystals ( $> 1$  mm) contain  
124 scattered melt inclusions.

125 Single crystals, optically free of flux melt inclusions, were selected for use in the solubility studies. Each  
126 crystal was first ground into spherical shapes with a diameter of  $\sim 1 - 2$  mm using 400-grit emery paper to  
127 remove sharp edges, and then rolled in 800-grit emery paper until they acquired a polish. The polished  
128 crystals were cleaned in ethanol in an ultrasonic bath, and then dried at 120 °C for 15 min. This procedure  
129 generated single crystals that ranged in weight from 0.7 to 3.0 mg (Table 1). Each experiment consisted of  
130 an outer Pt capsule (outer diameter: 3.0 mm, thickness: 0.2 mm) and an inner Pt capsule (outer diameter:  
131 2.0 mm, thickness: 0.1 mm) in which the monazite or xenotime single crystal was placed. Thick-walled Pt  
132 (0.2 mm) was used for the outer capsule to minimize puncturing by the thermocouple. The use of an inner  
133 capsule protected the crystal and minimized thermal gradients in the capsule (Tropper and Manning,  
134 2005). After inserting the crystal, the inner capsule was lightly crimped to facilitate H<sub>2</sub>O penetration while  
135 ensuring crystal containment during the experiments. The inner Pt capsule, plus precisely weighed  
136 quantities of KCl and H<sub>2</sub>O (Table 1), were then placed in the outer Pt capsule. The outer Pt capsule was  
137 sealed by arc-welding and then placed in a 120 °C oven for 30 min to check for leakage.

138 All experiments were performed at 800 °C and 1000 MPa in a non end-loaded piston-cylinder apparatus,  
139 using 22 mm diameter NaCl assemblies with a cylindrical graphite oven and sealed by pyrophyllite rings.  
140 Each double capsule assembly was placed horizontally at the center of the NaCl assembly surrounded by  
141 the graphite-furnace and packed in NaCl. It was covered with a small, thin pyrophyllite sheet to help  
142 prevent puncture by the thermocouple which is in direct contact with the Pt capsule. Pressure and  
143 temperature was monitored using a pressure gauge and a NiCr-Ni thermocouple, respectively. Pressure  
144 was maintained to within 200 bar gauge pressure and the accuracy of the reported temperature is estimated  
145 to be  $\pm 2$  °C. Each experiment was initially brought to 0.2 GPa and 100 °C and held for 15 min, then  
146 brought to 800 °C and 1.0 GPa following a temperature and pressure ramp of 20 °C/min and 0.02  
147 GPa/min. After 12 h, the experiments were quenched to  $T < 150$  °C and  $P < 0.6$  GPa within several  
148 seconds by shutting off the power to the graphite oven. Run times of 12 h for each experiment at 800 °C  
149 and 1.0 GPa were assumed sufficient to ensure significant reaction and equilibration of the monazite or

150 xenotime starting crystals with the solution. Attainment of constant solubility within 12 h is consistent  
151 with equilibration rates in other solubility measurements at high T and P, based on previous studies (e.g.,  
152 Caciagli and Manning, 2003; Tropper and Manning, 2005; Tropper et al., 2011).

153 After each experiment, the outer capsule was pierced with a needle, and the pH of the quench fluid was  
154 checked with a pH-indicator paper with an accuracy of < 0.5 pH units (Table 1). After drying for 30 min  
155 at 120 °C, the monazite or xenotime crystal was then extracted from the inner capsule, treated  
156 ultrasonically in ethanol to remove adhering quench precipitate, dried at 120 °C, and weighed with a  
157 Mettler Toledo XP2U ultra-microbalance ( $1\sigma = 0.1 \mu\text{g}$ ) (Table 1). All monazite and xenotime grains were  
158 then examined optically with a binocular microscope. Single crystals from selected experiments were  
159 mounted onto double-sided carbon tape and characterized by a JEOL JSM-6010LV scanning electron  
160 microscope (SEM) equipped with a Quantax EDS (Bruker).

161 The solubility of monazite and xenotime is reported in parts/million by weight (ppm), and is calculated via  
162 the formulas  $(\Delta m_{\text{mz}} / \text{H}_2\text{O} + \text{KCl} + \Delta m_{\text{mz}}) * 10^6$  and  $(\Delta m_{\text{xt}} / \text{H}_2\text{O} + \text{KCl} + \Delta m_{\text{xt}}) * 10^6$ , where mz and xt  
163 stand for monazite and xenotime. Reported mole fractions of KCl ( $X_{\text{KCl}}$ ) were calculated from the starting  
164 ratio  $n_{\text{KCl}} / n_{\text{KCl}} + n_{\text{H}_2\text{O}}$  in the experiment. KCl and H<sub>2</sub>O masses were determined on a Mettler Toledo  
165 AX205 DeltaRange microbalance ( $1\sigma = 0.03 \text{ mg}$ ) (Table 1). For further speciation calculations the  
166 monazite and xenotime mass loss ( $\Delta m_{\text{mz}}$  and  $\Delta m_{\text{xt}}$ ) and the measured pH were used to calculate ionic  
167 species utilizing the concept of the limiting reactant (Table 2a, Table 2b).

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## Results

### 170 Textures and equilibrium

171 The experimental results are given in Table 1. Run products included partly dissolved starting monazite-  
172 (Fig. 1a) and xenotime crystals (Fig. 1c), recrystallized CePO<sub>4</sub> grains on the surface of monazite starting  
173 crystals (Fig. 1b), yttrium chloride crystals on the surface of xenotime starting crystals (Fig. 1d), newly  
174 formed secondary monazite- (Fig. 2a, Fig. 2b), xenotime- (Fig. 2c, Fig. 2d), and yttrium chloride crystals

175 (Fig. 2c) in the outer capsules of some experiments, and a sub-micron sized white powder consisting of  
176 KCl (Fig. 2). The chemical identification of the yttrium chloride crystals was done semi-quantitatively  
177 using EDS analysis on the scanning electron microscope (SEM). Despite the small grain size and their  
178 adherence to the crystal faces of the starting crystals EDS analysis showed distinct Y and Cl peaks only  
179 and based on the approximate ratio between Y and Cl of 1:1, we infer the stoichiometry of this compound  
180 to be  $\text{YCl}(\text{OH})_2$ . This quench phase most likely formed from the strongly hygroscopic phase  $\text{YCl}_3$ , which  
181 reacts directly with  $\text{H}_2\text{O}$  to  $\text{YCl}(\text{OH})_2$  and  $\text{HCl}$  based on the following chemical reaction:  $1 \text{YCl}_3 + 2 \text{H}_2\text{O}$   
182  $= 1 \text{YCl}(\text{OH})_2 + 2 \text{HCl}$  (Klevtsova & Klevtsov, 1965; Haschke, 1975; Zhuravleva et al., 2013). Tropper et  
183 al. (2011) postulated for the system xenotime- $\text{H}_2\text{O}$ - $\text{NaCl}$  that a similar simple equilibrium could account  
184 for this relationship namely:  $\text{YPO}_4 + \text{NaCl} + 2\text{H}_2\text{O} = \text{YCl}(\text{OH})_2 + \text{NaH}_2\text{PO}_4$ . The residual monazite- and  
185 xenotime crystals displayed solution-rounded edges (Fig. 1a, Fig. 1c) and in some cases, significant  
186 dissolution grooves (Fig. 1a). The recrystallized  $\text{CePO}_4$  grains on the surface of the monazite starting  
187 crystals occur as idiomorphic, prismatic, tabular – granular aggregates (Fig. 1b) and quench crystals occur  
188 as tiny, round precipitates, which were distributed randomly on the surface of the xenotime starting  
189 crystals (Fig. 1d). The newly formed euhedral secondary monazite and xenotime crystals occur as hollow,  
190 prismatic needles (Fig. 2), which are randomly distributed throughout the inner and outer capsules. The  
191 abundance of secondary monazite and xenotime needles increased with increasing  $X_{\text{KCl}}$ , accompanied by  
192 an increase in monazite or xenotime solubility (Table 1). The size of the secondary monazite crystals was  
193 up to  $\sim 15 \mu\text{m}$  along the c-axis (Fig. 2a, Fig. 2b), the size of the secondary xenotime crystals was up to  $\sim 5$   
194  $\mu\text{m}$  along the c-axis (Fig. 2c, Fig. 2d). Both secondary monazite and xenotime crystals vary from sparse  
195 and separate crystallites to fibrous aggregates which were mostly embedded in KCl aggregates (Fig. 2).  
196 Two generations of secondary monazite quench crystals with different size and morphology (Fig. 2b)  
197 were found in the system monazite- $\text{H}_2\text{O}$ -KCl at a mole fraction of  $X_{\text{KCl}} = 0.1$ . The first generation of  
198 monazites (sec mz I) can be recognized by its characteristic prismatic crystals (Fig. 2a, Fig. 2b). The  
199 second generation of monazites (sec mz II) occurs as stellate clusters of thin needles, which are



200 significantly smaller than the monazite crystals of the first generation. In addition to the secondary  
201 monazite and xenotime crystals, < 2  $\mu\text{m}$  tabular – prismatic grains of  $\text{YCl}(\text{OH})_2$  crystals were observed in  
202 the system xenotime- $\text{H}_2\text{O}$ -KCl at a mole fraction of  $X_{\text{KCl}} = 0.1$ , embedded in KCl aggregates (Fig. 2c).  
203 Based on the textural observations, it can be assumed that the newly formed secondary monazite,  
204 xenotime, and yttrium chloride crystals nucleated and grew during quenching to room temperature from  
205 the experimental T, whereas the KCl aggregates precipitated during drying after initial puncturing of the  
206 outer capsule. The attribution of these secondary phases as quench material is in accordance with previous  
207 observations from similar experiments (e.g., Tropper and Manning, 2005, 2007a,b; Antignano and  
208 Manning, 2008, Tropper et al., 2011). No evidence for vapor-transport of monazite or xenotime was  
209 observed, unlike in some mineral-fluid systems such as calcite, rutile, and corundum (Caciagli and  
210 Manning, 2003; Tropper and Manning, 2005, 2007b) or fluorapatite in the system  $\text{NaCl} + \text{H}_2\text{O}$  (Antignano  
211 and Manning, 2008).

212

### 213 **Monazite solubility in $\text{H}_2\text{O}$ -KCl**

214 The experimental results in the system monazite- $\text{H}_2\text{O}$ -KCl are given in Table 1 and shown in Fig. 3a. At  
215 800  $^\circ\text{C}$  and 1.0 GPa, the solubility of the synthetic monazite in pure  $\text{H}_2\text{O}$  is 8 ppm (Table 1) (Tropper et  
216 al., 2011). The solubilities of synthetic monazite in  $\text{H}_2\text{O}$ -KCl fluids indicate an increase in the dissolved  
217 monazite concentration with rising  $X_{\text{KCl}}$  from  $78 \pm 4$  ppm ( $X_{\text{KCl}} = 0.101$ ) to  $335 \pm 3$  ppm ( $X_{\text{KCl}} = 0.506$   
218 (Table 1). The data on the variation in synthetic monazite solubility with  $X_{\text{KCl}}$  at 1.0 GPa and 800  $^\circ\text{C}$  (Fig.  
219 3a) can be fit to a second-degree polynomial function using least squares regression:

$$220 \quad c_{\text{mz}} = -464 X_{\text{KCl}}^2 + 891 X_{\text{KCl}} + 8 \quad (1)$$

221 where  $c_{\text{mz}}$  is the solubility of the synthetic monazite in ppm ( $R^2 = 0.986$ ) and  $X_{\text{KCl}}$  is the mole fraction of  
222 KCl. It can be also seen from Figure 3a that at  $X_{\text{KCl}} = 0.262$ , the solubility of natural monazite ( $186 \pm 3$   
223 ppm) (Table 1) fits well to the data of synthetic monazite solubility. In contrast to the  $\text{H}_2\text{O}$ -KCl system,  
224 monazite solubilities are considerably higher in the  $\text{H}_2\text{O}$ -NaCl system as shown by Tropper et al. (2011).

225 Their results also indicate an increase in the dissolved monazite concentration with rising  $X_{\text{NaCl}}$  to near  
226 halite saturation from 152 ppm ( $X_{\text{NaCl}} = 0.092$ ) to 442 ppm ( $X_{\text{NaCl}} = 0.498$ ) (Fig. 3a). The increase in the  
227  $\text{CePO}_4$  solubility with increasing NaCl concentration is similar to that seen for apatite, fluorite, calcite,  
228 anhydrite (Antignano and Manning, 2008; Tropper and Manning, 2007a; Newton and Manning, 2002;  
229 Newton and Manning, 2005) and monazite in the system  $\text{H}_2\text{O}$ -KCl. In addition, the quench pH of the  
230 aqueous solutions in the monazite- $\text{H}_2\text{O}$ -KCl experiments was 7.0 – 7.5 (Table 1).  
231 Figure 4 and Figure 5 show the relationship between the molality of monazite vs. the mole fraction of KCl  
232 ( $X_{\text{KCl}}$ ) and the activity of  $\text{H}_2\text{O}$  at 800°C and 1.0 GPa. The molality of the monazite is reported in mol/kg,  
233 and is calculated from the amount of substance ( $n_{\text{mz}}$ ) divided by the mass of  $\text{H}_2\text{O} + \text{KCl}$ . The  $\text{H}_2\text{O}$  and  
234 KCl activities were calculated using the Aranovich and Newton (1996, 1997) NaCl-KCl a-X formulation.  
235 Aranovich and Newton (1997) found that the KCl component lowers  $a_{\text{H}_2\text{O}}$  even more than NaCl at a given  
236 T, P, and  $X_{\text{H}_2\text{O}}$ , and that the KCl activity is lower for a given salt concentration than the NaCl activity  
237 (Aranovich and Newton, 1996). At 1.0 GPa, the solutions closely approach an ideal fused salt mixture,  
238 where the activities of  $\text{H}_2\text{O}$  and KCl correspond to an ideal activity formulation. The low  $\text{H}_2\text{O}$  activity at  
239 high pressures in concentrated KCl solutions indicates that such solutions should be feasible as chemically  
240 active fluids capable of coexisting with solid rocks in many deep crustal and upper mantle metamorphic  
241 and metasomatic processes (Aranovich and Newton, 1996).

242

### 243 **Xenotime solubility in $\text{H}_2\text{O}$ -KCl**

244 The experimental results for the system xenotime- $\text{H}_2\text{O}$ -KCl are given in Table 1 and shown in Fig. 3b. In  
245 pure  $\text{H}_2\text{O}$  at 800°C and 1.0 GPa, the solubility of synthetic xenotime is 46 ppm (Table 1) and is thus ~ 6  
246 times higher than for synthetic monazite (8 ppm) (Table 1; Tropper et al., 2011). The solubilities of  
247 synthetic xenotime in  $\text{H}_2\text{O}$ -KCl fluids show an increase in the dissolved xenotime concentration with  $X_{\text{KCl}}$   
248 increasing from  $67 \pm 5$  ppm ( $X_{\text{KCl}} = 0.099$ ) to  $126 \pm 4$  ppm ( $X_{\text{KCl}} = 0.348$ ) (Table 1) (Fig. 3b). At  $X_{\text{KCl}} >$   
249 0.348 the solubility of xenotime decreases to  $122 \pm 5$  ppm ( $X_{\text{KCl}} = 0.493$ ) (Fig. 3b). The data can be fit

250 using a second-degree polynomial function to describe the synthetic xenotime solubility as a function of  
251  $X_{\text{KCl}}$  at 800°C and 1.0 GPa (Fig. 3b):

$$252 \quad c_{\text{xt}} = -563 X_{\text{KCl}}^2 + 432 X_{\text{KCl}} + 46 \quad (2)$$

253 where  $c_{\text{xt}}$  is the solubility of synthetic xenotime in ppm ( $R^2 = 0.921$ ) and  $X_{\text{KCl}}$  is the mole fraction of KCl.  
254 Again xenotime solubilities are considerably higher in the system H<sub>2</sub>O-NaCl as shown by Tropper et al.  
255 (2011) where the dissolved xenotime concentration increases with rising  $X_{\text{NaCl}}$  from 173 ppm ( $X_{\text{NaCl}} =$   
256 0.096) to 265 ppm ( $X_{\text{NaCl}} = 0.286$ ) (Fig. 3b). At  $X_{\text{NaCl}} > 0.286$  the solubility decreases to 212 ppm ( $X_{\text{NaCl}} =$   
257 0.399) and 191 ppm ( $X_{\text{NaCl}} = 0.496$ ) (Fig. 3b). YPO<sub>4</sub> solubility in the system H<sub>2</sub>O-NaCl by Tropper et al.  
258 (2011) increases in a manner similar to that of corundum and wollastonite (Newton and Manning, 2006),  
259 and shows a different trend than the solubility of YPO<sub>4</sub> in the system H<sub>2</sub>O-KCl (Fig. 3b). Similar to the  
260 monazite-H<sub>2</sub>O-KCl experiments, the xenotime-H<sub>2</sub>O-KCl experiments have neutral quench pH values of 7  
261 – 7.5 over the investigated  $X_{\text{KCl}}$  range (Table 1).

262 Figure 4 and Figure 5 show the relationship between the molality of xenotime vs. the mole fraction of KCl  
263 ( $X_{\text{KCl}}$ ) and the activity of H<sub>2</sub>O at 800°C and 1.0 GPa.

264

265

## Discussion

### 266 Monazite and xenotime solubility as a function of $X_{\text{salt}}$ at 800°C and 1.0 GPa

267 The low solubility of monazite and xenotime in pure H<sub>2</sub>O experimentally obtained by Tropper et al.  
268 (2011) makes it difficult to explain the natural association of these minerals with metasomatic features in  
269 igneous and metamorphic rocks, such as hydrothermal alteration assemblages, veins, and skarns (e.g.,  
270 Gieré, 1996). The fluid flux must be high enough to mobilize relatively insoluble REE, in which the  
271 solubility of (Y+REE) orthophosphates is low in near-neutral pH aqueous fluids and increases in acidic  
272 fluids (e.g. Tropper et al., 2013). An alternative mechanism for the dissolution and transportation of  
273 orthophosphate components is a high NaCl and/or KCl concentration in the fluid phase. Tropper et al.  
274 (2011) found that YPO<sub>4</sub> solubility in pure H<sub>2</sub>O at 800°C and 1 GPa is greater (46 ppm) than that of CePO<sub>4</sub>

275 (8 ppm). This is in nominal disagreement with the general observation that monazite is more common  
276 than xenotime in hydrothermal veins and other metasomatic features, which implies greater solubility of  
277 LREE relative to HREE and Y (e.g., Schmidt et al., 2007), and suggests that LREE are more abundant  
278 than HREE in such systems. However, REE and Y dissolution in natural fluids are controlled by ligands  
279 other than H<sub>2</sub>O or phosphate, such as chloride, fluoride, and sulfate, all of which can be expected to occur  
280 in varying proportions (e.g., Williams-Jones et al., 2012). Consequently, experimental results obtained  
281 using pure H<sub>2</sub>O only represent an end-member scenario unlikely to occur in nature.

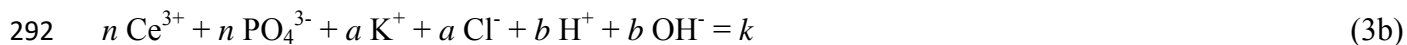
282 To obtain information on the interaction of monazite and xenotime with pure H<sub>2</sub>O and KCl + H<sub>2</sub>O  
283 solutions, the following generalized dissolution reactions may be written (Newton and Manning, 2006,  
284 2010; Tropper and Manning, 2011):



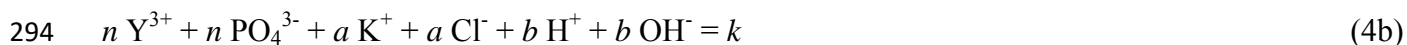
286 or



288 where  $n$  are the number of moles of monazite or xenotime, and  $a$  and  $b$  are the number of moles of KCl  
289 and H<sub>2</sub>O consumed to produce  $k$  moles of solutes per mole of orthophosphate dissolved. The  $k$  moles of  
290 solutes per mole of orthophosphate were calculated assuming complete dissociation. The dissociation is  
291 represented by the following equations (Aranovich and Newton, 1996; Newton and Manning, 2006):



293 or



295 The relative molar proportions of KCl and H<sub>2</sub>O in Eqs. (3a) and (4a) were evaluated using the technique  
296 outlined in Newton and Manning (2006, 2010). In case that the solubility of monazite or xenotime  
297 decreases with  $X_{\text{KCl}}$ , then  $\text{Ce}^{3+}$  or  $\text{Y}^{3+}$  solutes would likely be hydrous species, and there would be no  
298 interaction with  $\text{K}^+$  and/or  $\text{Cl}^-$ . Similarly, monotonic increase with  $X_{\text{KCl}}$  would imply no interaction with

299  $H^+$  and/or  $OH^-$ . If monazite and xenotime solubility increases to a plateau - like maximum and then  
300 declines this would imply that their solutes include both hydrates and K- and/or Cl complexes. Figure 6a  
301 and Figure 6b shows the variations in the relative solubility enhancements of synthetic monazite and  
302 xenotime, expressed as a solute mole fraction for a given  $X_{KCl}$  relative to that in pure  $H_2O$ . The effect of  
303 KCl on monazite and xenotime solubility can be assessed from the log-ratios  $X_{mz} / X_{mz}^\circ$  and  $X_{xt} / X_{xt}^\circ$ ,  
304 where  $X_{mz}^\circ$  and  $X_{xt}^\circ$  are the mole fractions of monazite and xenotime in pure  $H_2O$ . The ratio  $\log X/X^\circ$   
305 thus represents the magnitude of solubility enhancement by a given KCl mole fraction.  
306 Values of  $\log X/X^\circ$ , especially for synthetic monazite in KCl solutions, increase with increasing  $X_{KCl}$  over  
307 the investigated range and this implies that the activity of  $H_2O$  does not significantly influence monazite  
308 solubility ( $b = 0$  in Eqn. 3a). This and the positive dependence of solubility on the square of  $X_{KCl}$  (Eqn. 1)  
309 suggests that 3 moles of KCl per mole of  $CePO_4$  form anhydrous solute species upon dissolution ( $a = 3$ ).  
310 A simple chemical equilibrium that could account for this relationship is:



312 The observed dissolution products in the KCl-bearing fluids are newly formed secondary monazite (Fig.  
313 2a, Fig. 2b),  $CeCl_3$ , and  $K_3PO_4$  (Eqn.5). Tropper et al. (2011) postulated that for the system monazite-  
314  $H_2O$ -NaCl a similar simple equilibrium could account for this relationship namely:  $CePO_4 + 2NaCl =$   
315  $CeCl_2^+ + Na_2PO_4^-$ . Table 2a represents a chemical reaction model of the system monazite- $H_2O$ -KCl, in  
316 which the quantified reaction products of  $CeCl_3$  and  $K_3PO_4$  are listed.

317 In contrast to monazite, the values of  $\log X/X^\circ$  for the synthetic xenotime are not sufficiently precise to  
318 define a maximum as in the NaCl system by Tropper et al. (2011). Nevertheless, the data rise with  
319 increasing  $X_{KCl}$  over the investigated range to a maximum at  $X_{KCl}$  between 0.35 and 0.45 (Fig. 6b). This  
320 implies that the activities of KCl and  $H_2O$  significantly influence xenotime solubility. Following the  
321 approach of Newton and Manning (2006), the KCl mole fraction, at which the maximum solubility occurs,  
322 defines the ratio of a to b in Eqn. 6 via:

323 
$$X_{\text{KCl}}^* = \frac{a}{a+b} \quad (6)$$

324 and implies that a (for KCl) is 3 and b (for H<sub>2</sub>O) varies between 5.5 ( $X_{\text{KCl}} = 0.35$ ) and 3.6 ( $X_{\text{KCl}} = 0.45$ )

325 (Fig. 6b). A simple chemical equilibrium that could account for this relationship at  $X_{\text{KCl}} = 0.43$  is:



327 where a = 3 and b = 4. The reaction products in the KCl-bearing fluids are YCl(OH)<sub>2</sub> (Fig. 1d, Fig. 2c),  
328 KH<sub>2</sub>PO<sub>4</sub>, KOH and HCl (Eqn. 7). The reverse reaction is defined as a neutralization reaction and occurs  
329 during the quenching process, in which the acid (HCl) and the base (KOH) react to form H<sub>2</sub>O and KCl and  
330 the H<sup>+</sup> combines with OH<sup>-</sup> to generate H<sub>2</sub>O. This results in a quench pH equal to 7.

331 The dissolution products proposed in Eqs. (5) and (7) suggest that, in NaCl- and also KCl bearing fluids  
332 with neutral pH, the degree of Cl coordination for Y is lower than for Ce (Tropper et al., 2011). Assuming  
333 similar geochemical behavior for Y and REE, this is consistent with the steric hindrance of chloride  
334 complexation with HREE relative to LREE proposed by Mayanovic et al. (2009). The common  
335 occurrence of NaCl- and KCl-rich fluids in crustal and mantle settings (e.g., Newton et al., 1998; Yardley  
336 and Graham, 2002; Newton and Manning, 2010) could offer a simple mechanism to explain numerous  
337 cases of LREE mobility. Table 2b represents a chemical reaction model for the system xenotime-H<sub>2</sub>O-  
338 KCl, in which the quantified reaction products of YCl(OH)<sub>2</sub> and KH<sub>2</sub>PO<sub>4</sub> are listed.

339

340

### Geological implications

341 Field studies of high-grade rocks show that the mobility of REE and Y in granulite-facies terranes is  
342 greatly enhanced in the presence of brines (e.g., Newton et al., 1998; Harlov, 2011; Aranovich et al.,  
343 2014) since brine-bearing fluid inclusions have been observed in granulites (e.g., Markl et al., 1998). It  
344 has therefore been proposed that REE (and by extension, Y) mobility may be enhanced by dissolved  
345 halogens in some cases as highly concentrated brines (e.g., Pan and Fleet, 1996; Schmidt et al., 2007;  
346 Antignano and Manning, 2008; Newton and Manning, 2010; Tropper et al., 2011, 2013). KCl brines or K-

347 rich fluids in the lower crust and upper mantle are, because of their high mechanical mobility and alkali-  
348 exchanging potential feasible metasomatic fluids for a variety of high grade rocks (Hansen et al., 1995;  
349 Newton et al., 1998; Harlov et al., 1998; Harlov and Förster, 2002a). Field observations (e.g., Touret and  
350 Nijland, 2013) and experimental investigations (Harlov, 2004) have demonstrated that a typical  
351 metasomatic feature associated with the presence of a high-salinity low-H<sub>2</sub>O activity fluid is the presence  
352 of K-feldspar veining along the grain boundaries of minerals such as quartz, biotite, and plagioclase.  
353 Tropper et al. (2011) experimentally determined the solubility of CePO<sub>4</sub> monazite and YPO<sub>4</sub> xenotime in  
354 H<sub>2</sub>O–NaCl solutions at 800 °C and 10 kbar. Their results indicate that the solubility of both Ce and Y  
355 increase with rising X<sub>NaCl</sub>. Moreover, it has been shown that the most saline solutions exhibit a strong  
356 preference for LREE over HREE (Reed et al., 2000) and additional experiments in the system NaF–H<sub>2</sub>O  
357 by Tropper et al. (2013) found that NaF solutions yielded an even stronger increase in Ce/Y concentration  
358 with rising salt concentrations. The present experiments in the system KCl–H<sub>2</sub>O strongly corroborate the  
359 NaCl–H<sub>2</sub>O experiments although the extent of solubility is lower. These experimental results help to  
360 explain key features of REE geochemistry in high-grade metamorphic processes since brine-induced  
361 anatexis will result in a noticeable depletion in the bulk REE concentration compared to parental rocks  
362 without the presence of brines as well as a decrease in the LREE/HREE ratio in the residual rock from  
363 which the melt was extracted.

364 Another important aspect is large-scale metasomatism involving brines. Metasomatic alteration is  
365 conjectured to involve infiltrating NaCl- and KCl-bearing brines during peak metamorphism as well as  
366 post peak and possibly more H<sub>2</sub>O-rich fluids during uplift and cooling. Alkali-halide brines play an  
367 important role in mass transport (e.g. K-metasomatism) and mineral-fluid-melt phase equilibria in the  
368 lower crust (e.g., Newton et al., 1998; Yardley and Graham, 2002; Harlov and Förster, 2002a; Newton and  
369 Manning, 2010). With respect to the formation of large-scale ore deposits the experimental results by  
370 Harlov et al. (2002a), Taghipour et al. (2015) and Harlov et al. (2016) also support the extensive  
371 metasomatic alteration and remobilization of REE-enriched iron-oxide-apatite (IOA) deposits due to the

372 presence of brine-rich fluids. This fact is corroborated by a number of experiments, which have shown  
373 that the formation of monazite and xenotime associated with apatite is a metasomatically induced process  
374 that results from the interaction of brine-rich fluids that are reactive with the (Y + REE)-bearing apatite  
375 (Harlov et al., 2002b; 2005; Harlov and Förster, 2003; Harlov, 2015; Harlov et al., 2016). These examples  
376 clearly show that further experimental investigations are still needed to understand the behavior of  
377 (Y+REE) carriers such as monazite and xenotime in the presence of brine-rich fluids, which frequently  
378 accompany high-grade metamorphism and metasomatic processes.

379

380

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386



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604 **Figure captions**

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606 **Figure 1.** SEM images of run products from selected experiments. (a)  $\text{CePO}_4$  crystal after  
607 dissolution at  $X_{\text{KCl}} = 0.101$  (Mnz\_003). (b) Surface of the  $\text{CePO}_4$  crystal dissolved in  $X_{\text{KCl}} =$   
608 0.101, displaying dissolution grooves and recrystallization. (c)  $\text{YPO}_4$  crystal after dissolution at  
609  $X_{\text{KCl}} = 0.348$  (Xnt\_028). (d)  $\text{YPO}_4$  crystal after dissolution in  $X_{\text{KCl}} = 0.099$  (Xnt\_023) fluid, with  
610 tiny quench crystals ( $\text{YCl}(\text{OH})_2$ ) adhering to the surface.

611 **Figure 2.** SEM images of the quench material from selected experiments. (a,b) Two generations  
612 of secondary monazite crystals, that occur as prismatic needles (sec mz I) and stellate clusters  
613 (sec mz II), which nucleated in the outer casule upon quench and embedded in KCl aggregates.  
614 (c,d) Tabular – prismatic crystal of  $\text{YCl}(\text{OH})_2$  and secondary xenotime crystals (sec xt), which  
615 embedded in KCl aggregates.

616 **Figure 3a.** Monazite solubility versus the mole fraction of KCl and NaCl ( $X_i$ ) at 800°C and 1.0  
617 GPa. The error bars are  $2\sigma$  and are calculated based on the weighing uncertainties. The solid line  
618 in the system monazite-KCl- $\text{H}_2\text{O}$  represents the fitted solubilities from Eqn. (1). Results of  
619 Tropper et al. (2011) from monazite-NaCl- $\text{H}_2\text{O}$  at 800°C and 1.0 GPa shown for comparison.  
620 Halite- and sylvite saturation estimated from Aranovich and Newton (1996, 1997).

621 **Figure 3b.** Xenotime solubility versus the mole fraction of KCl and NaCl ( $X_i$ ) at 800°C and 1.0  
622 GPa. The error bars are  $2\sigma$  and are calculated based on the weighing uncertainties. The solid line  
623 in the system xenotime-KCl- $\text{H}_2\text{O}$  represents the fitted solubilities from Eqn. (2). Results of  
624 Tropper et al. (2011) from xenotime-NaCl- $\text{H}_2\text{O}$  at 800°C and 1.0 GPa shown for comparison.  
625 Halite- and sylvite saturation estimated from Aranovich and Newton (1996, 1997).

626

627 **Figure 4.** The relation between the molality of monazite and xenotime vs. the mole fraction of  
628 KCl and NaCl ( $X_i$ ) at 800°C and 1.0 GPa. Results of Tropper et al. (2011) from monazite and  
629 xenotime in the system NaCl-H<sub>2</sub>O at 800°C and 1.0 GPa are shown for comparison. Halite- and  
630 sylvite saturation estimated from Aranovich and Newton (1996, 1997).

631 **Figure 5.** The relation between the molality of monazite and xenotime in the system H<sub>2</sub>O-KCl vs.  
632 the activity of H<sub>2</sub>O at 800°C and 1.0 GPa.

633 **Figure 6a.** Logarithm of the solubility enhancement of monazite,  $X_{mz}/X_{mz}^{\circ}$ , versus  $X_{KCl}$  at 800°C  
634 and 1.0 GPa. Values of  $\log X_{mz}/X_{mz}^{\circ}$  increase continuously with increasing  $X_{KCl}$  over the  
635 investigated range and this implies that the activity of H<sub>2</sub>O does not significantly influence  
636 monazite solubility ( $b=0$ ). This suggests that 3 moles of KCl per mole of CePO<sub>4</sub> form anhydrous  
637 solute species upon dissolution ( $a=3$ ).

638 **Figure 6b.** Logarithm of the solubility enhancement of xenotime,  $X_{xt}/X_{xt}^{\circ}$ , versus  $X_{KCl}$  at 800°C  
639 and 1.0 GPa. Values of  $X_{xt}/X_{xt}^{\circ}$  rise with increasing  $X_{KCl}$  over the investigated range to a  
640 maximum at  $X_{KCl}$  between 0.35 and 0.45. This implies that the activities of KCl and H<sub>2</sub>O  
641 significantly influence xenotime solubility and that  $a$  (for KCl) is 3 and  $b$  (for H<sub>2</sub>O) varies  
642 between 5.5 ( $X_{KCl} = 0.35$ ) and 3.6 ( $X_{KCl} = 0.45$ ).

643

644

## Tables

645 **Table 1:** Experimental results in the system Monazite-H<sub>2</sub>O-KCl and Xenotime-H<sub>2</sub>O-KCl at  
 646 800°C and 1.0 GPa

Run number	Time (h)	H <sub>2</sub> O in (mg)	KCl in (mg)	X <sub>KCl</sub>	Crystal in (mg)	Crystal out (mg)	Solubility (ppm)	pH
<b>Synthetic Monazite - H<sub>2</sub>O - KCl</b>								
Mnz-18*	90	35.89	0.00	0.000	1.1635	1.1632	8	-
Mnz_003	12	35.20	16.44	0.101	2.8190	2.8150	78 (4)	7.0
Mnz_005	12	31.01	23.11	0.153	2.6666	2.6603	116 (2)	7.0
Mnz_013	12	21.77	31.44	0.259	1.3995	1.3872	232 (6)	7.5
Mnz_012	12	14.08	38.07	0.395	1.6765	1.6615	288 (8)	7.0
Mnz_015	12	9.08	38.50	0.506	1.0983	1.0823	335 (3)	7.5
<b>Natural Monazite - H<sub>2</sub>O - KCl</b>								
Mnz_017	12	21.31	31.38	0.262	1.2343	1.2245	186 (3)	8.0
<b>Synthetic Xenotime - H<sub>2</sub>O - KCl</b>								
Xnt-4*	12	41.62	0.00	0.000	2.3541	2.3522	46	-
Xnt_023	12	34.60	15.81	0.099	0.8727	0.8693	67 (5)	7.0
Xnt_024	12	25.59	27.31	0.205	0.9871	0.9805	124 (1)	7.5
Xnt_028	12	16.31	36.07	0.348	0.9329	0.9263	126 (4)	7.5
Xnt_027	12	10.47	42.17	0.493	0.7068	0.7004	122 (5)	7.5

647

648 Explanation: “Crystal in” and “Crystal out” refer respectively to the weights before and after the experiment. Weights reported to two decimal  
 649 places were determined on a Mettler Toledo AX205 DeltaRange microbalance ( $1\sigma = 0.03$  mg); those to four places were determined on a Mettler  
 650 Toledo XP2U ultra microbalance ( $1\sigma = 0.1$   $\mu$ g). The solubility is expressed with the  $1\sigma$  uncertainty, based on propagation of weighing errors. Run  
 651 numbers Mnz-18 and Xnt-4, which are marked with a star, are the experiments in pure H<sub>2</sub>O at 800°C and 1.0 GPa from Tropper et al. (2011).

652

653 **Table 2a:** Chemical reaction model of the system monazite-H<sub>2</sub>O-KCl. Based on the limiting  
 654 reactant approach for monazite, the dissolution reaction  $1 \text{ CePO}_4 + 3 \text{ KCl} = 1 \text{ CeCl}_3 + 1 \text{ K}_3\text{PO}_4$   
 655 occurs over the investigated range of  $X_{\text{KCl}}$  (0.101 – 0.506) and implies no interaction with H<sub>2</sub>O.  
 656 The amount of water remains unchanged before and after the chemical reaction ( $m \text{ H}_2\text{O} = m \text{ H}_2\text{O}$   
 657 rest)

<b>Monazite - KCl</b> $1 \text{ CePO}_4 + 3 \text{ KCl} =$					$1 \text{ CeCl}_3 + 1 \text{ K}_3\text{PO}_4$				
Run number	$\Delta m \text{ CePO}_4$ [ $\mu\text{g}$ ]	$m \text{ H}_2\text{O}$ [mg]	$m \text{ KCl}$ [mg]	$X_{\text{KCl}}$	$m \text{ CeCl}_3$ [ $\mu\text{g}$ ]	$m \text{ K}_3\text{PO}_4$ [ $\mu\text{g}$ ]	$m \text{ H}_2\text{O rest}$ [mg]	$m \text{ KCl rest}$ [mg]	obs pH
<b>Mnz_003</b>	4.05	35.20	16.440	<b>0.101</b>	4.25	3.66	35.20	16.436	7.0
Run number	$\Delta m \text{ CePO}_4$ [ $\mu\text{g}$ ]	$m \text{ H}_2\text{O}$ [mg]	$m \text{ KCl}$ [mg]	$X_{\text{KCl}}$	$m \text{ CeCl}_3$ [ $\mu\text{g}$ ]	$m \text{ K}_3\text{PO}_4$ [ $\mu\text{g}$ ]	$m \text{ H}_2\text{O rest}$ [mg]	$m \text{ KCl rest}$ [mg]	obs pH
<b>Mnz_013</b>	12.35	21.77	31.440	<b>0.259</b>	12.95	11.15	21.77	31.428	7.5
Run number	$\Delta m \text{ CePO}_4$ [ $\mu\text{g}$ ]	$m \text{ H}_2\text{O}$ [mg]	$m \text{ KCl}$ [mg]	$X_{\text{KCl}}$	$m \text{ CeCl}_3$ [ $\mu\text{g}$ ]	$m \text{ K}_3\text{PO}_4$ [ $\mu\text{g}$ ]	$m \text{ H}_2\text{O rest}$ [mg]	$m \text{ KCl rest}$ [mg]	obs pH
<b>Mnz_015</b>	15.98	9.08	38.503	<b>0.506</b>	16.75	14.42	9.08	38.487	7.5

658

659

660 **Table 2b:** Chemical reaction model of the system xenotime-H<sub>2</sub>O-KCl. Based on the limiting  
 661 reactant approach for xenotime, the dissolution reaction  $1 \text{ YPO}_4 + 4 \text{ H}_2\text{O} + 3 \text{ KCl} = 1 \text{ YCl(OH)}_2$   
 662  $+ 1 \text{ KH}_2\text{PO}_4 + 2 \text{ HCl} + 2 \text{ KOH}$  occurs over the investigated range of  $X_{\text{KCl}}$  (0.35 – 0.45) and  
 663 implies an interaction with KCl and H<sub>2</sub>O. The corresponding amounts of water and salt change  
 664 accordingly after the chemical reaction ( $m \text{ H}_2\text{O} > m \text{ H}_2\text{O rest}$  and  $m \text{ KCl} > m \text{ KCl rest}$ )

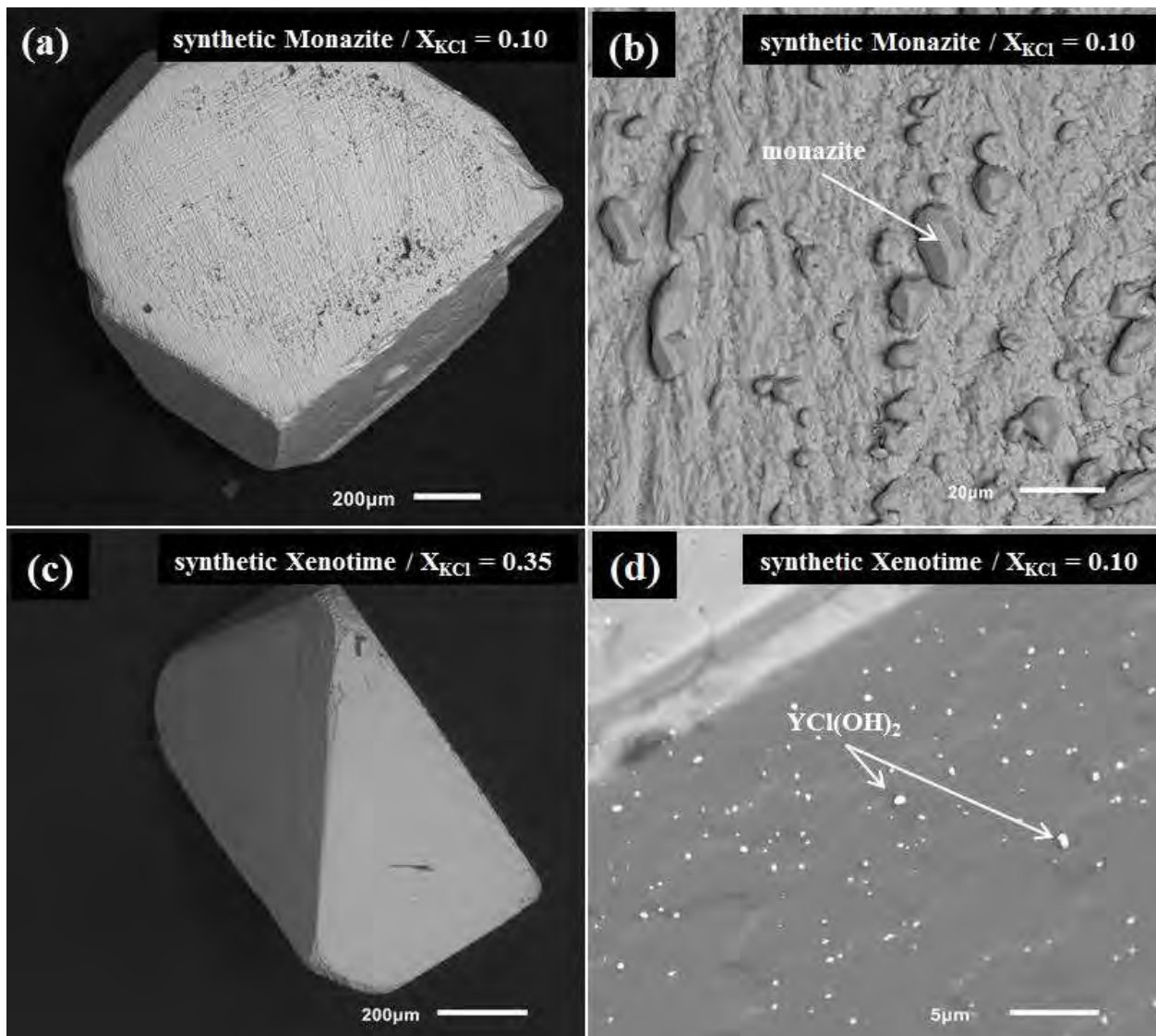
<b>Xenotime - H<sub>2</sub>O - KCl</b> $1 \text{ YPO}_4 + 4 \text{ H}_2\text{O} + 3 \text{ KCl} =$					$1 \text{ YCl(OH)}_2 + 1 \text{ KH}_2\text{PO}_4 + 2 \text{ HCl} + 2 \text{ KOH}$						
Run number	$\Delta m \text{ YPO}_4$ [ $\mu\text{g}$ ]	$m \text{ H}_2\text{O}$ [mg]	$m \text{ KCl}$ [mg]	$X_{\text{KCl}}$	$m \text{ YCl(OH)}_2$ [ $\mu\text{g}$ ]	$m \text{ KH}_2\text{PO}_4$ [ $\mu\text{g}$ ]	$m \text{ HCl}$ [ $\mu\text{g}$ ]	$m \text{ (KOH)}$ [ $\mu\text{g}$ ]	$m \text{ H}_2\text{O rest}$ [mg]	$m \text{ KCl rest}$ [mg]	obs pH
<b>Xnt_028</b>	6.60	16.310	36.070	<b>0.348</b>	5.68	4.88	2.62	4.03	16.307	36.062	7.5
Run number	$\Delta m \text{ YPO}_4$ [ $\mu\text{g}$ ]	$m \text{ H}_2\text{O}$ [mg]	$m \text{ KCl}$ [mg]	$X_{\text{KCl}}$	$m \text{ YCl(OH)}_2$ [ $\mu\text{g}$ ]	$m \text{ KH}_2\text{PO}_4$ [ $\mu\text{g}$ ]	$m \text{ HCl}$ [ $\mu\text{g}$ ]	$m \text{ (KOH)}$ [ $\mu\text{g}$ ]	$m \text{ H}_2\text{O rest}$ [mg]	$m \text{ KCl rest}$ [mg]	obs pH
<b>Xnt_027</b>	6.40	10.468	35.500	<b>0.493</b>	5.51	4.74	2.54	3.91	10.465	35.492	7.5

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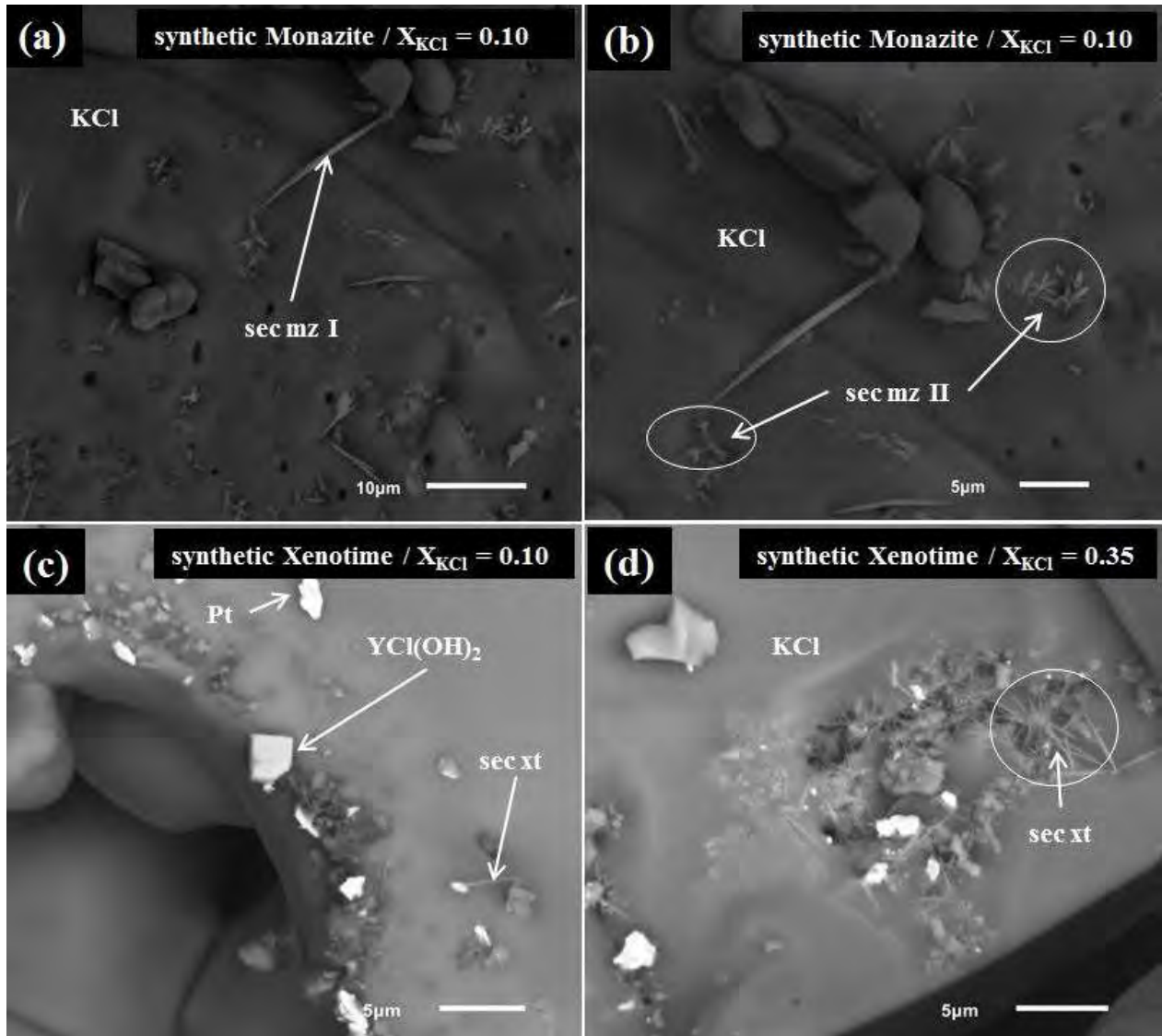
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Figures



668 **Figure 1.**

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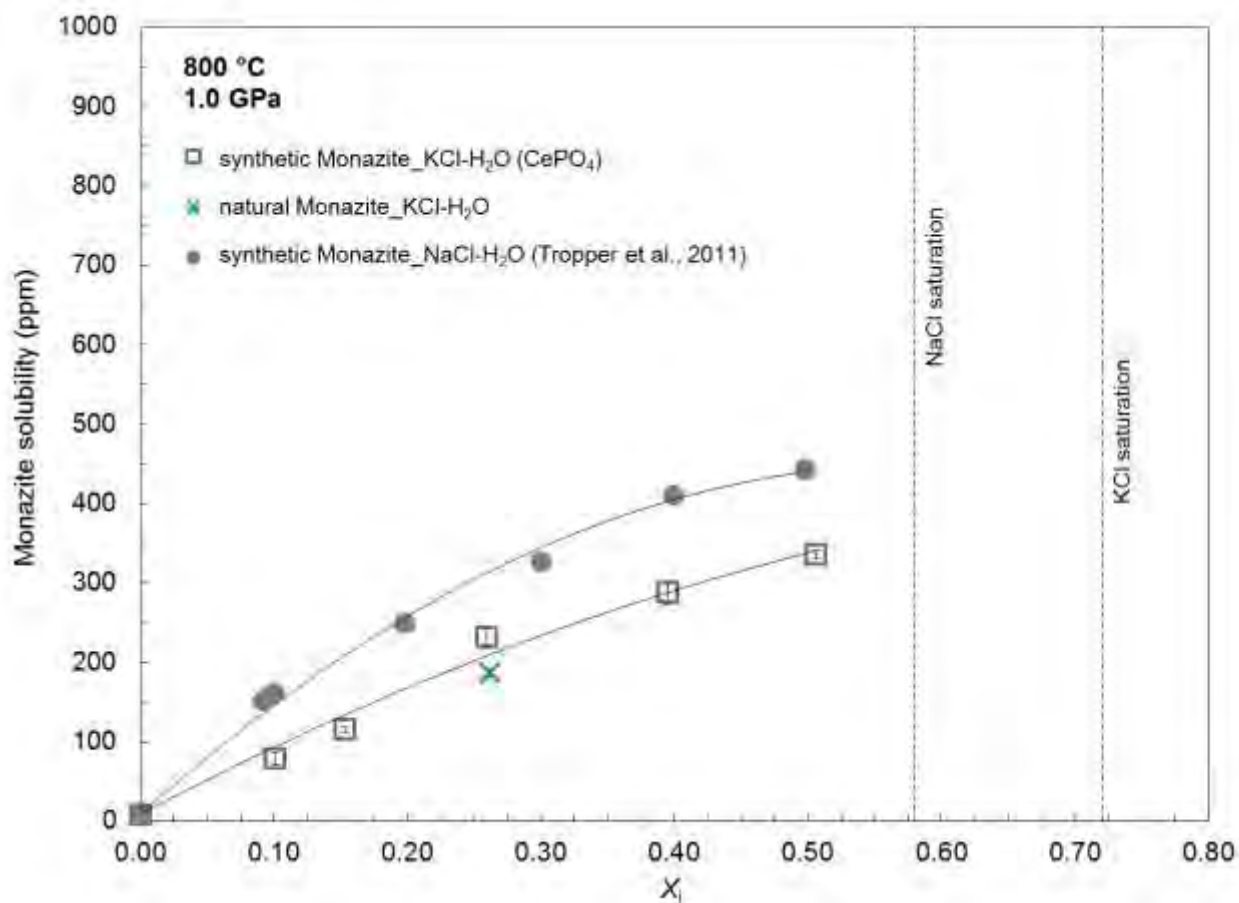
671 **Figure 2.**

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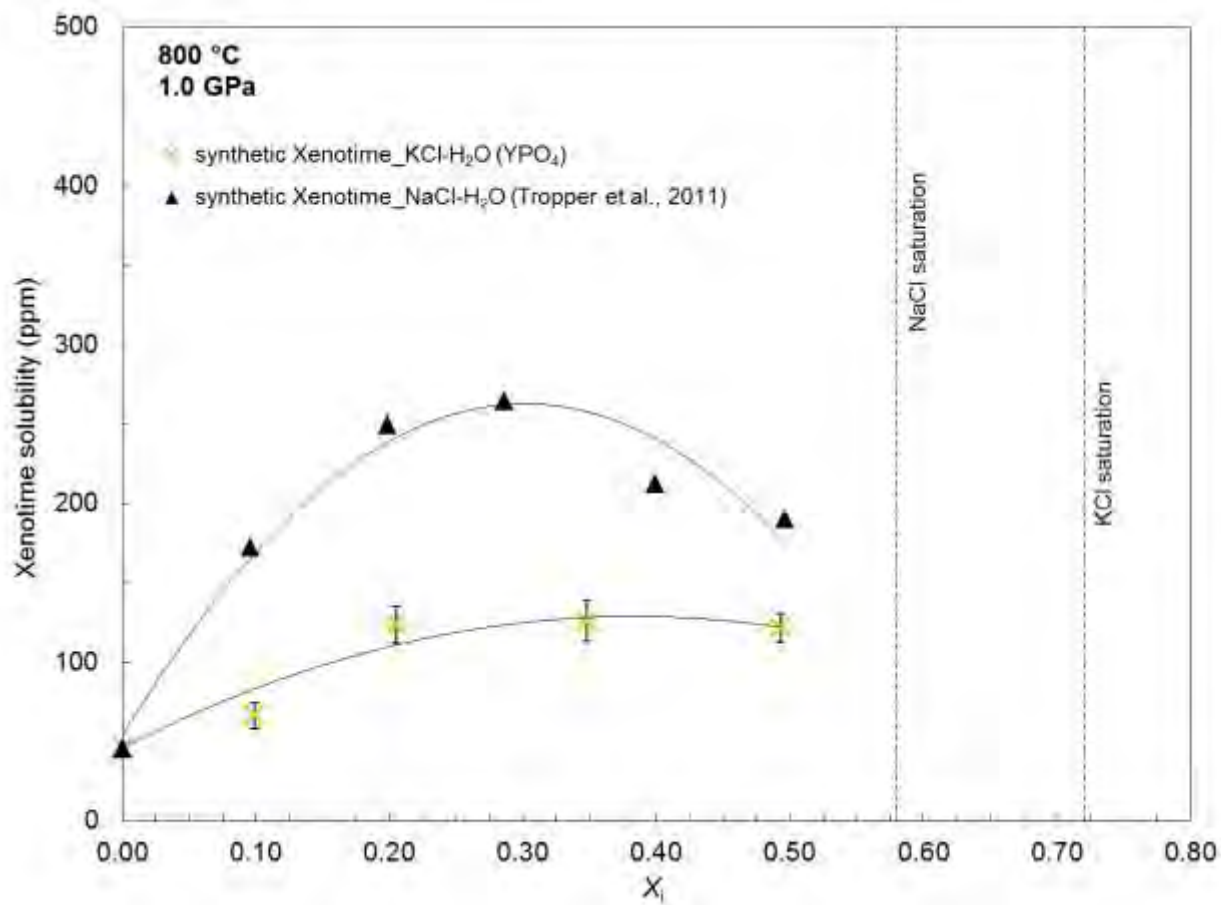




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676 **Figure 3a.**

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679 **Figure 3b.**

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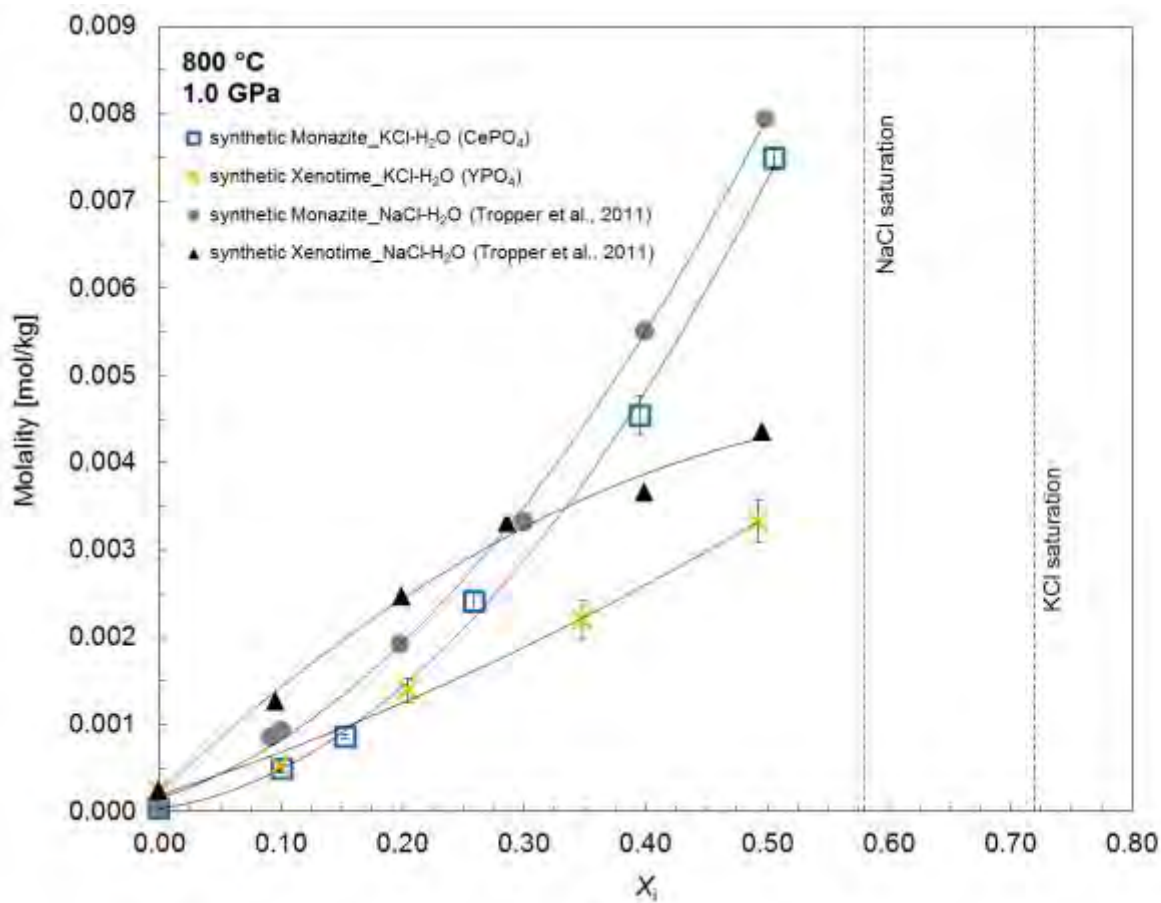
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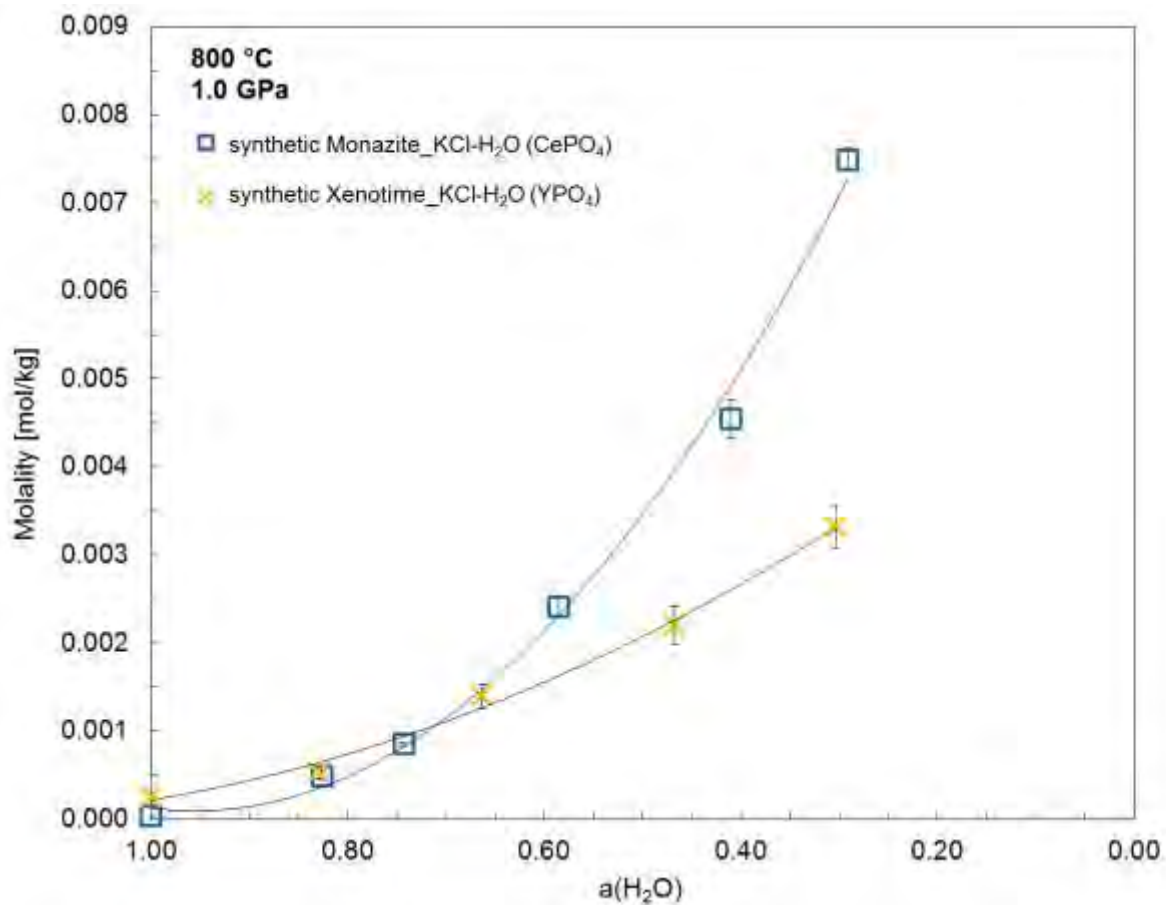


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687 **Figure 4.**

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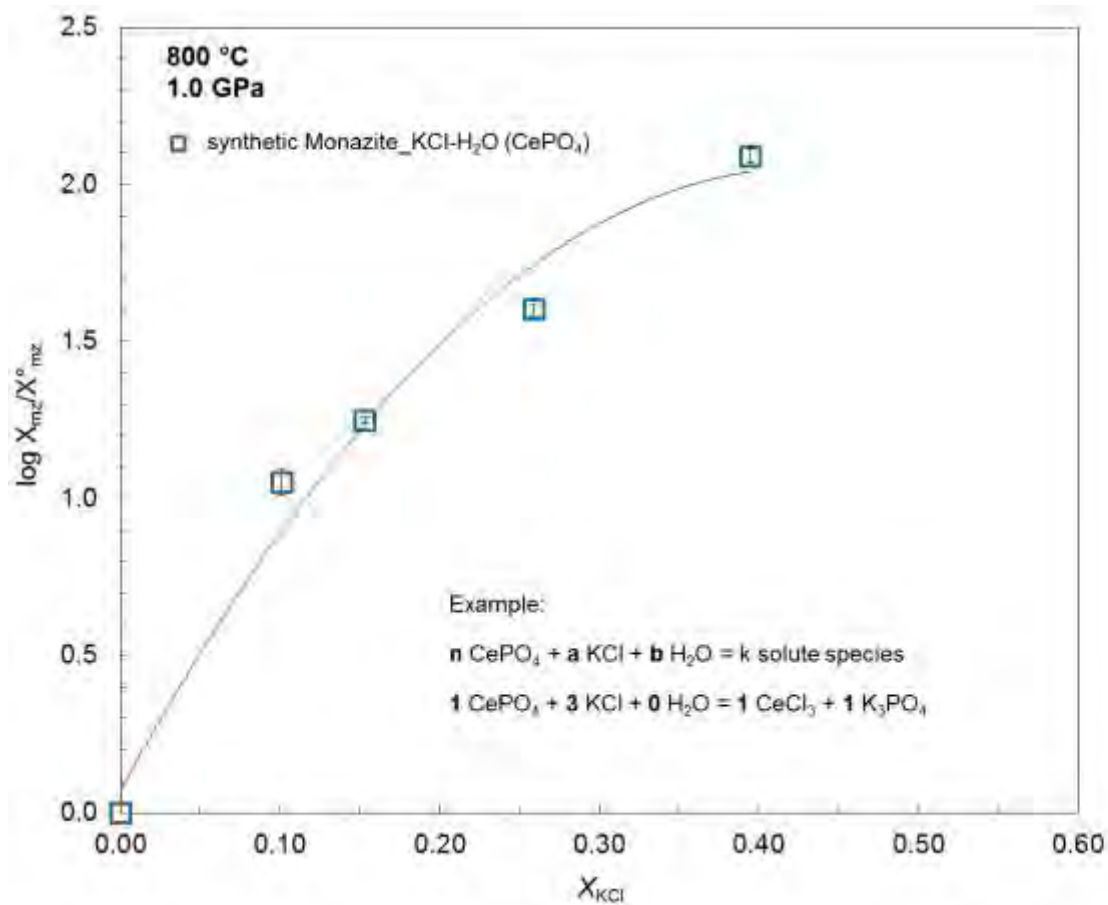


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691 **Figure 5.**

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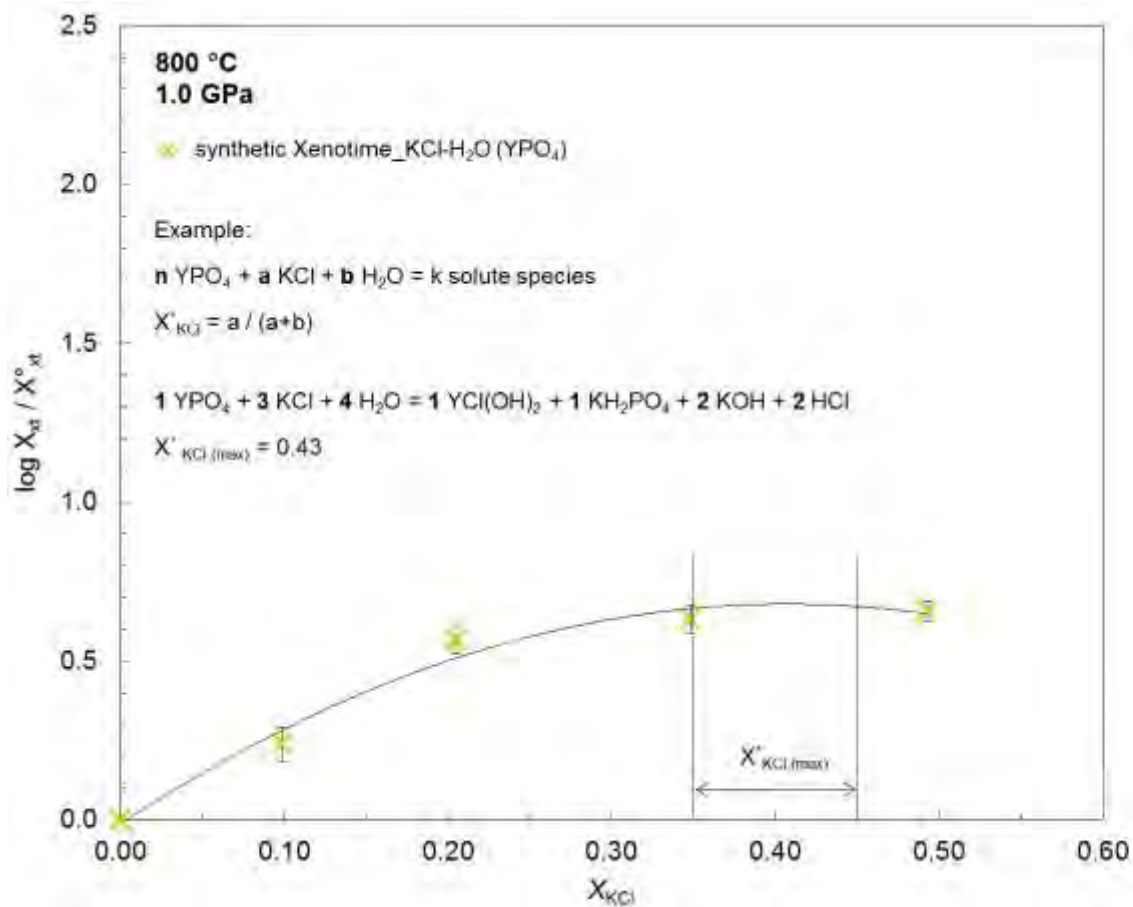


694  
695 **Figure 6a.**

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Figure 6b.